Improving Flash Gas Emission Calculations from Storage Tanks

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Significant Methane Emission Sources in Oil and Gas Production (Gg)



Activity	2005	2007	2008	2009	2010	2011
Oil Production Field Operations	1,366	1,396	1,407	1,432	1,443	1,475
Pneumatic Device Venting	398	398	416	419	416	428
Tank Venting	188	193	185	202	211	221
Combustion & Process Upsets	71	72	75	94	95	99
Wellhead Fugitives	19	20	24	23	22	24
Misc. Venting and Fugitives	690	714	706	694	700	702
Natural Gas Systems	7,572	8,018	7,782	7,178	6,838	6,893
Field Production	3,595	3,958	3,640	2,948	2,724	2,545
Processing	667	723	756	834	787	932
Transmission & Storage	1,879	1,942	1,964	2,021	1,980	2,087
Source: Inventory of U.S. Greenhouse Gas Emi	ssions and Sin	ks: 1990-2011	L – Tables 3-37	2 & 3-44 (EPA 4	130-R-13-001,	04-12-2013)

Flash Gas Emissions from Oil and Gas Production Facilities



- Flash gas is produced when pressure applied to produced liquids is lowered
- Flash gas may arise from both oil and water
- Normal methods for quantifying flash gas are:
 - Vasquez-Beggs Equation (simple mathematics)
 - API E&P Tanks Program (iterative calculations)
 - Process simulation software (HYSIS, PROMAX, etc.)
 - Measurements
- Specific data are required by each approach
- Assumptions may be made regarding certain data or operating conditions
- Accuracy of results depends on the input data available

Challenges to Accurate Predictions



- Data needs for each method are specific
- Sampling of several production phases may be necessary to obtain the required model inputs
- Laboratory speciation analysis followed by calculation of mixture parameters provides model inputs
- Collecting representative samples of multi-phase materials is a major concern
- Sampling may be simple compared to analysis
- Other sources of gas emissions may be vented to tanks
 - Glycol dehydrator vents
 - Other process vents, including prior separator stages
 - Process upsets (stuck dump valves, maintenance venting, etc.)

Sampling Approach



- Determine the composition data required
 - What are the conditions at the final pressure drop?
 - Which gas streams are vented, flared or used as fuel?
 - What streams have significant potential for fugitive emissions?
 - Are multiple product streams combined prior to an emission point?
 - What quality assurance/control checks are needed for the data produced?
- Identify other data necessary for performing the flash gas calculation method selected
- Use a sketch of the facility to identify the piping diagram (showing process fluid flows) and each sample location

Flash Gas Emission Sources



NaturalGas

Data Requirements for E&P Tanks



• Physical Data

- Separator temperature (°F)
- Separator pressure (psig)
- Ambient temperature (°F)
- Ambient pressure (psia)
- Facility location (latitude/longitude or UTM coordinates)
- Separator throughput (bbls/day)

Chemical Data

- Composition and GOR of high-pressure or low-pressure oil
- Composition of high-pressure gas
- Molecular weight and specific gravity for oil and gas samples
- API gravity and Reid vapor pressure of oil samples

Other

Operating Schedule (days/year)

E&P TANKS Set-up Options



E&P TANK - Untit	led. Ept		
File View Unit Convers	sion Run Help		
0 🛩 🖬 🎒 📸	61 🕵 %	💕 🥐	
	Project Setup	roject Description	
	Flowsneet Set	ectori	Model Selection for was Losses
Project Setup	-\$+C	Tank with Separator	C AP-42 (uses methodologies documented in EPA AP-42)
	-	C Stable Oil Tank	RVP Distillation Column
Data Insul	⊏ Known Senar	ator Stream Information	Control Efficiency
Data Input	i chown oopu	C 1 Law Pressure Oil	
			Use Control Efficiency
		C 2. High Pressure Oil	
	U	3. Low Pressure Gas	8
Data Output		G Geographical Databa	ase
	4-1-1		
	Air Injection		
	Ĵ <u></u> ↓	🔲 Enter Air Compositio	on for Air/Gas Injection

Input & Output Screens





Data Inputs for High or Low Pressure Oil



-{	Free 23.	rator Conditio ssure 0	ons [psig]	-Low P	Fessure Oil Sep Pre 23	Input arator Conditi assure 3.0	ons [psig]	Low P	ressure Oil I	nput arator Condit	ons	Temperati	ITO
omp lo.	Component	mol %	~	Comp	positions			-	23	.0	(psig)	85.0	[F]
	H2S	0.0508		No	Component	mol %		_		1	Ŧ	~	
2	02	0.0000		10	HC5	3 1066		Comp	iositions			C10+ Chara	cterization
3	C02	0.2437		11	n-C5	5.0558		No.	Component	mol %	~	Item	Data
ļ.	N2	0.0102		12	106	4 1726		13	C7	10.3655		MW	166.00
5	C1	0.9543		13	C7	10.3655		14	C8	10.8426		SG	0.8990
Š.	C2	0.6701		14	C8	10.8426		15	C9	5.5127			
	C3	2.1827		15	C9	5 5127		16	C10+	45.9695			
1	i-C4	1.1269		16	C10+	45,9695		17	Benzene	0.5685			
1	n-C4	4.6091	-	17	Benzene	0.5685	_	18	Toluene	0.2132			
0	i-C5	3.1066	~	18	Toluene	0.2132	-	19	E-Benzene	0.0711			
otal	= 100.0000			19	E-Benzene	0.0711	V	20	Xylenes	0.6802			
No	rmalize		K)	Total	= 100.0000			21 22 Total	n-C6 224Trimethylp - 100 0000	3.5939 0.0000	~		

Data Inputs for Gas Phase



-0-	Pre 23	arator Conditio Issure .0	pris [psig]	Low Pi	ressure Gas I Separ Pres [23.1]	input ator Conditi sure D	ons [psig]	Temperatur 85.0	e[F]
Vo.	Component	mol %	~	-Comp				-Molar Pation	in Sen Dil-
	H2S	0.0000		L		1 100		Comment	In sept of
2	02	0.0075		No.	Component	mol %		Lomponent	Hatio
3	CO2	0.5145		10	1-1-5	0.7969	_		1.0000
4	N2	0.5329		11	n-L5	1.3635	_	10	1.0000
5	C1	76.5098		12	L6	0.2318	_	10	1:0000
6 1	C2	8.6730		13	C7+	0.6783	_	<u>[L10+</u>	1.0000
7	C3	7.6347		14	Benzene	0.0262	_	-C10, Charaol	lorization
3 i	i-C4	0.9855		15	Toluene	0.0273	_	CTO+ Charac	tenzation
3	n-C4	1.8224		16	E-Benzene	0.0051	_	Item	Data
10 i	i-C5	0.7969	~	17	Xylenes	0.0108		MW	166.00
otal =	100.0000			18	n-C6	0.1798		ISG	0.8990
GOR: F Data I Morm	Ratio of Separ Type folar GOR	rator Gas and Volumetric	GOR	Total GOR Dat	= 100.0000 : Ratio of Separa ta Type Molar GOR	ator Gas and Volumetric	d Separa GOR	tor Oil Molar GOR 0. Enter Volum	0500 netric GOR

Inputs for Physical Data



The flash valve is shown for illustration purposes only to indicate pressure reductions through a flow line. A calculation will be performed to flash the separator oil to the ambient condition	Sales Oil Input		
	Production Rate	2000	[bbl/day]
Ambient Pressure 14.7 [psia]	Days of Annual Operation	n 365	[days/year]
Ambient l'emperature 170.0	API Gravity	46.0	-
1 atmosphere pressure equals to 14.7 psia. If known, enter the ambient or tank inlet temperature. Otherwise, enter the upstream separator temperature.	Reid Vapor Pressure	7.70	[psia]

Laboratory Management Approach



- Work with the laboratory on sampling and analysis before sampling
- Tell the laboratory exactly what data are expected to be in the lab report
- Ensure that liquid sample analyses include at least
 C₁ through C₉ and C₁₀s+, HAPs, He, H₂, N₂, O₂, and CO₂
- Obtain data for H₂S and total sulfur for each phase or sample
- Report mole % and weight % for each constituent and molecular weight of each gas or liquid mixture

Continued on the next slide »

Laboratory Approach (continued)



- Calculate and report vapor pressure, specific gravity, API gravity, Reid vapor pressure, and GOR for liquid samples
- Calculate and report vapor density (or specific gravity), heat content (MMBtu/scf), and molecular weight of each gas
- Ensure that the requested analytical report covers data needed for other purposes (health risk impacts, GHG emission reports, etc.)
- Ensure that all field sampling data (separator temperatures and pressures, ambient temperature, and ambient pressure) are included in the lab report

Summary



- Calculating and reporting flash gas emission rates from oil and gas facilities can and should be improved
- Flash gas data are not only important for monitoring process emissions and documenting CH₄ reductions, but also for numerous other required emission calculations
- Involving the analytical laboratory prior to sampling helps ensure completeness of data for process modeling inputs
- Using good sampling and analysis procedures is important for ensuring quality results
- Things at the facility are not always what they appear to be, so document any unusual situations observed during the sampling process
- Process upsets happen and do not produce representative samples for performing emission calculations

Contact Information



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Questions?

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