

Regulation 13.7.1 Approved Method

Application: Ships constructed 1 Jan 1990 to 31 Dec 1999
Marine diesel engine power output >5,000 kW
Per cylinder displacement 90 litres

If a method has been approved by Party according to chapter 7 of the NOx Technical Code 2008 then ship is required to fit the “approved method” to enable the engine to meet Tier I limits.

IMO to be notified of approved method

**The approved method to be installed at first renewal survey
12 months or more after IMO notified the “method” is approved**

Tier	$n < 130$ rpm	$130 \leq n < 2000$ rpm	$n \geq 2000$ rpm
I	17.0 g/kWh	$45.0 \cdot n^{(-0.2)}$ g/kWh	9.8 g/kWh



Johnson Matthey
Catalysts

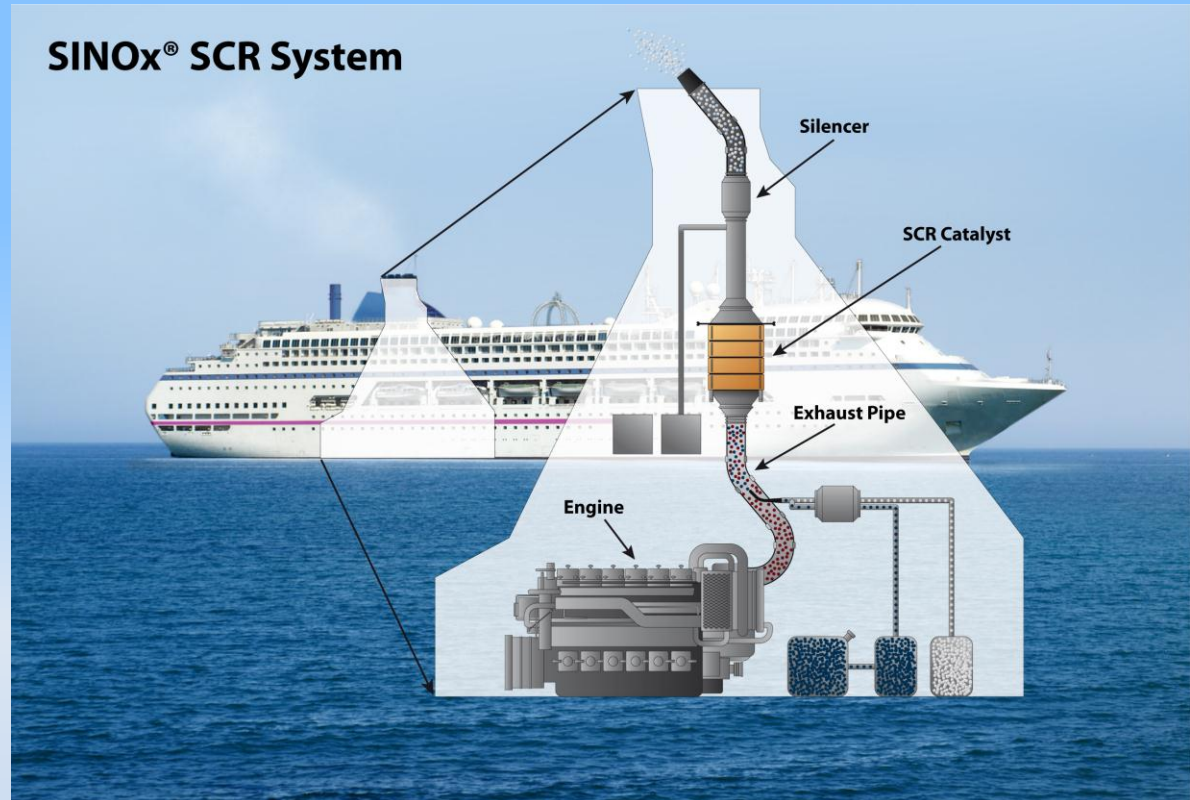
Technology for meeting IMO III NO_x limits

Mexico Sept 26th Sept

Joseph Mc Carney
Johnson Matthey



International
Association for
Catalytic
Control of
Ship
Emissions to
Air





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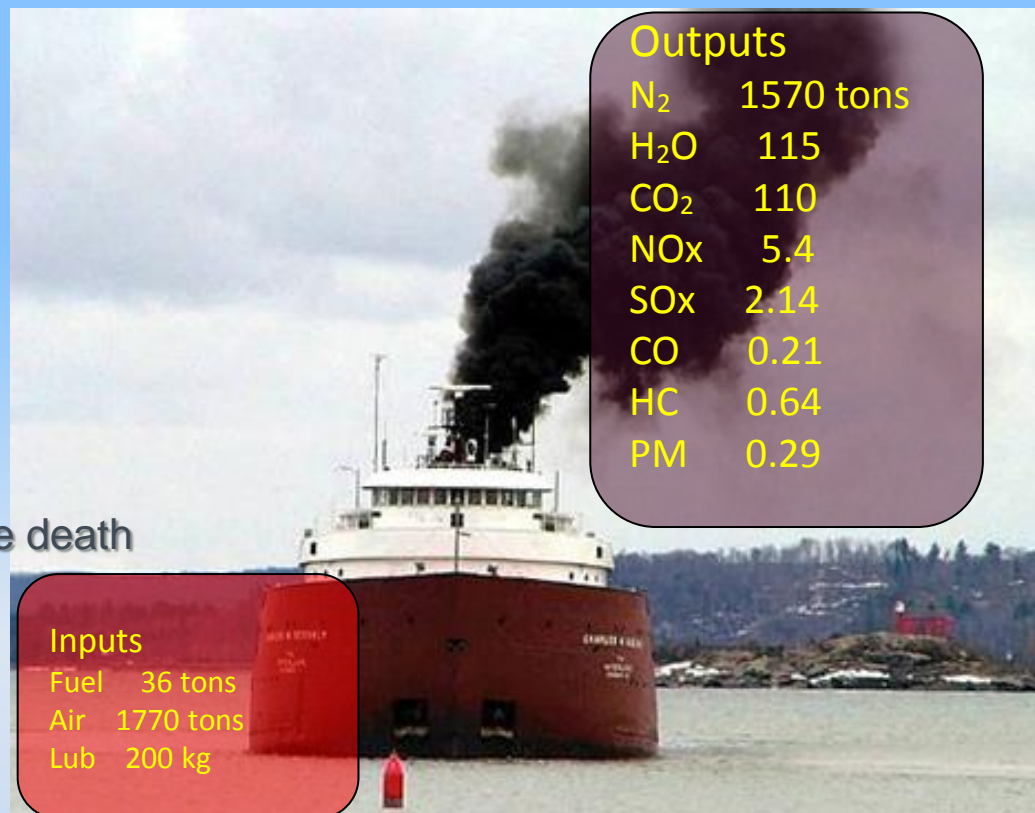
A Major Player

- **Speciality chemicals –advanced materials**
- **1817 1942 2002 2008 2012**
- **Core skills in Catalysis, PGMs & Process Tech.**
- **Invest in R&D and Manufacturing Technology**
- **Operate in over 30 countries, 10000 employees**
- **Focus on Growth Opportunities - environment**
- **Technology & Market Leadership**
- **160 SCR systems on ships – large and small**



A Major Contribution **NO_x**

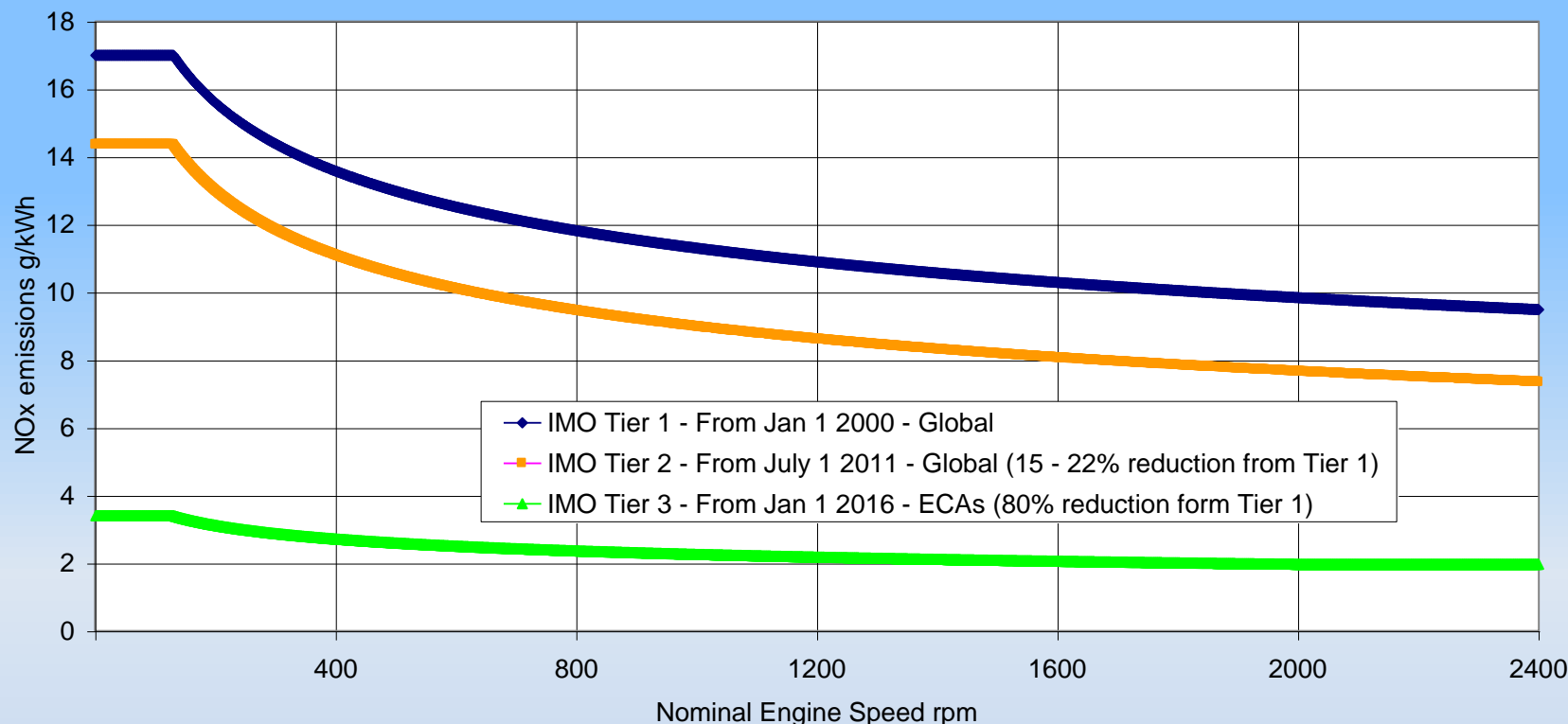
- Formed in the heat of the engine
- SMOG & Particulates
- Acidifies the environment
- Lung and heart disease
- Economic costs
 - Medical care
 - Lost Productivity
 - Cost of pain / ill health / premature death
- US EPA – ECA application
 - 14000 lives saved p.a
 - 5m experience relief – respiratory symptoms



A Major Requirement

“IMO Tier III scripted to force after-treatment in NO_x ECAs”

New IMO NO_x Regulations for New Constructions (EIAPP Reg 13)



◆ IMO Tier 1 - From Jan 1 2000 - Global
 ■ IMO Tier 2 - From July 1 2011 - Global (15 - 22% reduction from Tier 1)
 ▲ IMO Tier 3 - From Jan 1 2016 - ECAs (80% reduction from Tier 1)

“Beginning in 2012 and completed no later than 2013, the Organization shall review the status of the technological developments to implement the standards set forth in paragraph 5.1.1 of this regulation and shall, if proven necessary, adjust the time periods set forth in that subparagraph.”

Regulation 13.10 of Annex 13, Resolution MEPC 176 (58):

IMO Review-Terms of Reference

Exceptions & Exemptions

Range

NO_x Review
Of Technology Solutions
To Meet IMO III

Applicability & Suitability

Status / Readiness
Technology Trajectory
Supply Chain Issues

Contributors

Canada	Japan	BIMCO	ICOMIA
Denmark	Liberia	CLIA	ICS
Estonia	Netherlands	CSC	IMarEST
Finland	Norway	Euromot	INTERTANKO
France	Sweden	IACS	IPIECA
Germany	United Kingdom	IADC	OCIMF
Ireland	United States	IAPH	WSC
European Commission		Integer	IACCSEA

Disclaimer – The views set out in this document reflect the interpretation of the author – and do not necessarily concur with the interpretation of the IMO or other stakeholders

Technology Options

LNG

Fuel Combustion – controlled to
Low NOx

SCR

NH₃ neutralises NOx on Catalyst

Other

Water Based / Valve Timing / TC
Control combustion process in
Diesel engine - Low NOx

EGR

Lower O₂ content & lower
Combustion Temperatures

Technology Options

Meeting IMO III NOx limits

LNG

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Combustion Temperatures

Technology Options - SCR

State of Technology Readiness SCR

Issue / Concern

Operating Conditions
e.g. Temperature
Catalyst Fouling – ABS
Low Load Performance

SCR System - design
Catalyst Lifetime
Ammonia Slip
Small Vessels

Supply Chain Concerns
Urea

Response

Flexibility -
SCR reactor placement
Charge Air, Timing, Burner
Below 25% Load – SCR off

Experience-
>16000 hours / 2 years
Mobile, Stationary, Ships – 500
Compact SCR – Design Phase

Competitive Global Supply Chain
AUS 40 Standard
US Supply Chain - by 2014



Technology Options - EGR

State of Technology Readiness EGR

Issue / Concern

Technology Readiness
Combined with other technology?
Not available for most engines

H₂SO₄ / PM
Reagent / wash water

Response

Capability Demonstrated
High NO_x reduction – IMO III
Development Focus Engine OEMs

Low operating costs Mg(OH)₂

Scrubber
Developing Experience

Technology Options - LNG

State of Technology Readiness LNG

Issue / Concern

Low emissions – dependent on
Engine size / duty cycle / pilot fuel

Energy Density

Response

Experience
100's Gas engines – low emissions
20 Vessels
Meets IMO III
Lower Fuel Costs



Technology Options - Other

State of Technology Readiness – Other
VVT, 2Stage TC... Water Based...

Issue / Concern

Response

Not Tier III Compliant
30% - 50% - 65%
DWI – HAM – FE

Can be used in combination

Miller Timing
Decreased Power

Loss over come with 2-stage TC

Technology Options - summary

LNG

Fuel Combustion – controlled to
Low NO_x

Practical

SCR

NH₃ neutralises NO_x on Catalyst

Panacea

Other

Water Based / Valve Timing / TC
Control combustion process in
Diesel engine - Low NO_x

Partial

EGR

Lower O₂ content & lower
Combustion Temperatures

Potential

Conclusion / Insight

Technology to meet IMO III limits is available
There are a number of options / combinations

Greater collaboration between Engine OEMs and other technology providers will deliver efficient, economical, environmental solutions, for cleaner shipping

IACCSEA

Greater collaboration between technology providers and regulators will maximise the gain to society at an “efficient” cost

IACCSEA



SCR installation – Alice Austen

Engines: 2 x CAT 3516 A
Temperature: 752°F
NOx Reduction: < 3 g/kWh (~ 70%)
SCR installed: 2004



Staten Island Ferry (US)



SCR installation – MS Timbus

SINOx[®] Installed:	1999
Type	MaK 8M32 (Main)/ MAN 6L16/24 (Aux.)
Power	3,840kW / 540 kW (Aux.)
Exhaust Gas Flow	21,000 / 3,000 Nm³/h
Fuel	HFO / MDO
Temperature	320 / 336° C
Urea Consumption :	97 / 8 l/h (@40%)



Catalyst Type	SW 30 Honeycomb
Catalyst Volume	3 m³/engine (Main) 0.4 m³/engine (Aux.)
Exhaust NOx:	2g/kWh



SCR installation – Kleven

Project: Supply Vessel/Work ship Kleven
Exhaust gas flow: 8.790 m³/h
Engine type: 2 x MAN 6L 32/40, 2 x MAN 8L 21/31
Fuel: MGO
Temperature: 335° C
SINOx[®] Installed: 2007



Catalyst type: SW 40
Catalyst volume: 3.8 m³
NOx Reduction: 86%





SCR installation – LNG Carriers

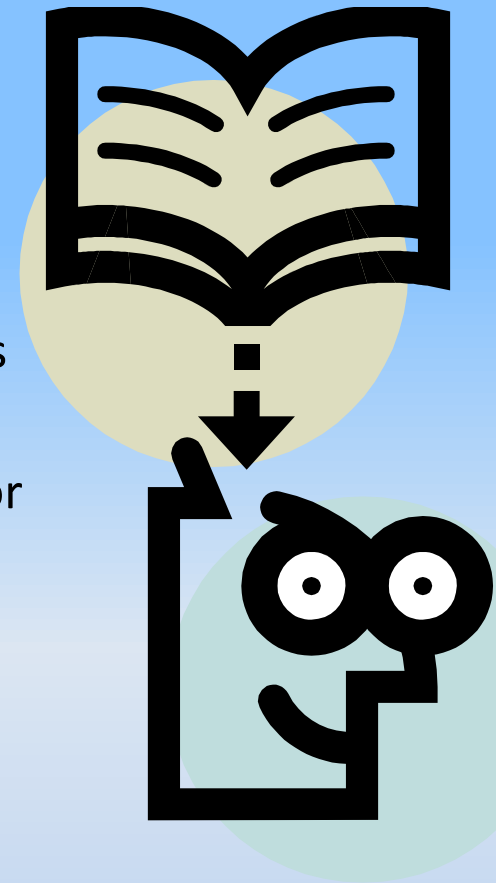
Project: 2 x LNG Carrier, Exmar Excellence/Excelerate
SINOx[®] Installed: 2007
Exhaust Gas Flow: 2 x 70.100 Nm³/h
Application: 2 x 70t/h Regas Boiler
Fuel: HFO/MDO
Temperature: 380°C



Catalyst Type: SW 30 Honeycomb
Catalyst Volume: 10,62 m³
Exhaust NOx : 30 mg/Nm³
Reduction Rate: 93%

De-NOx - Selective Catalytic Reduction

- 1. Combustion → pollution inc. the acidic pollutants - NOx & SOx
- 2. NOx is dangerous, & increasingly its emission is regulated.
- 3. NOx can be controlled in the engine or neutralised in the tailpipe – via catalytic after treatment such as SCR
- 4. SCR is a proven technology (power-plants, HDD and auto)
- 5. The SCR process produces Nitrogen as its end product
- 6. Marine SCR – >500 Case studies – yachts to container ships
- 7. SCR needs a reducing agent – Urea / Ammonia
- 8. The catalyst is robust but requires the correct conditions for optimum operation
- 9. Sulphur is not a poison to Marine SCR Catalysts – but its effects need to be considered – e.g. limiting temperature.
- 10. After-treatment can allow an increase in efficiency (fuel)
- 11. SCR on its own can meet IMO III or as a top up technology





Johnson Matthey
Catalysts

Technology for IMO III Mexico Sept 26th Sept

For Further information please contact

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